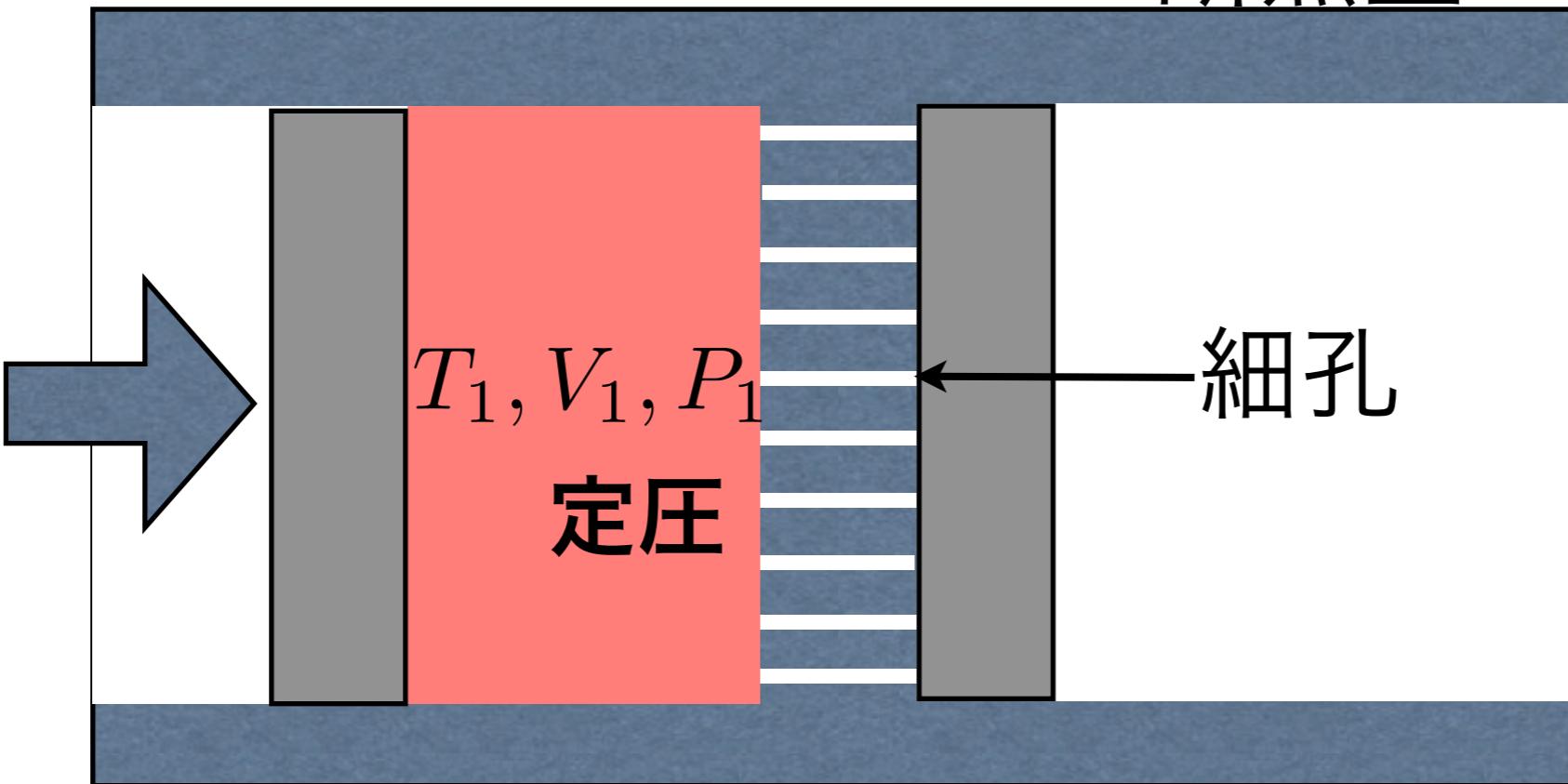


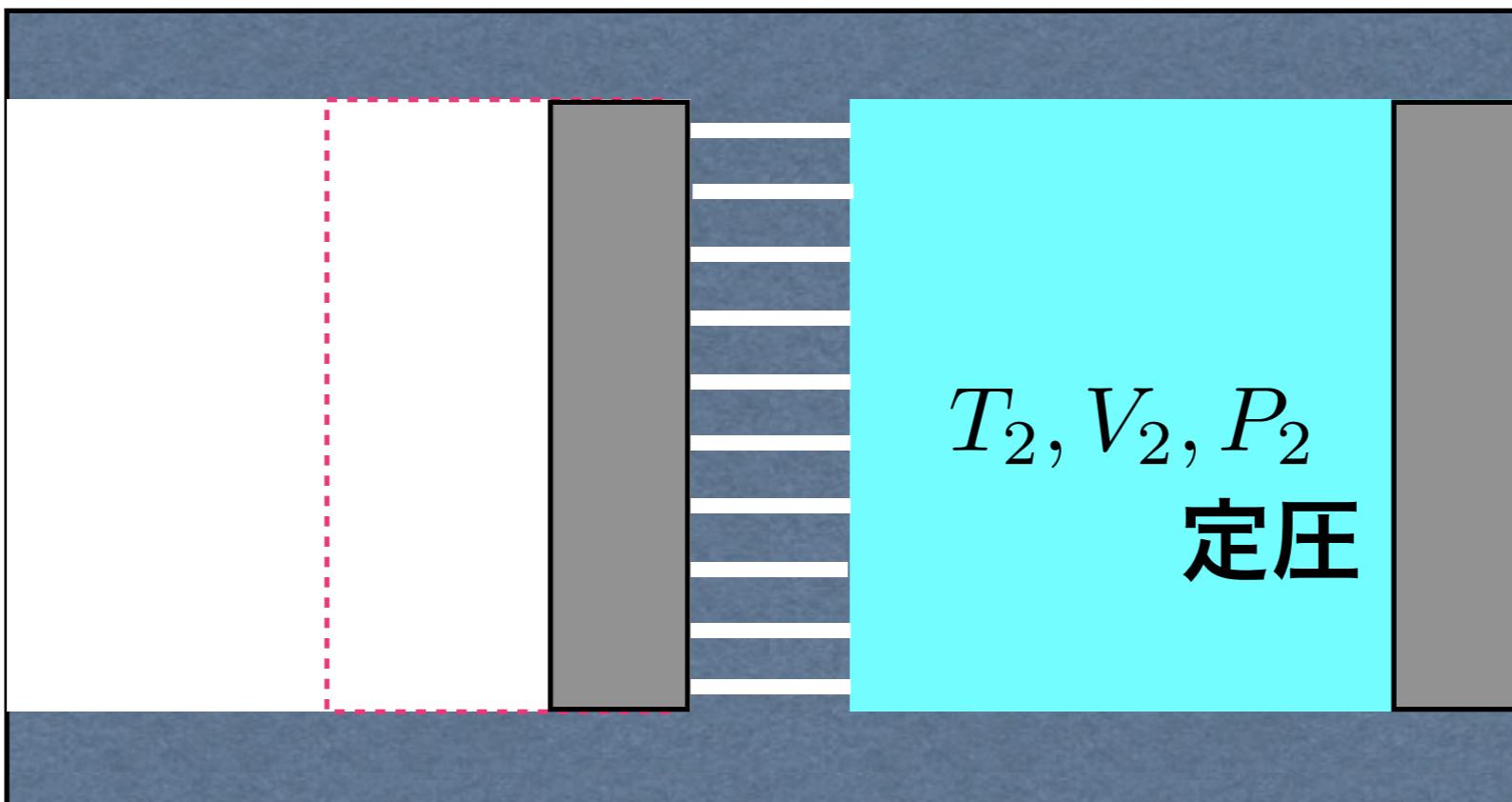
Joule-Thomson(Kelvin) : ガスの液化に使う

断熱壁

before



after



internal energy

	after	before
left:	0	U_1
right:	U_2	0
total :	$U_2 - U_1$	

気体が存在しなければ $U=0$

work

left:	$+P_1V_1$
right:	$-P_2V_2$
total:	$+P_1V_1 - P_2V_2$

気体は仕事をされた
気体は仕事をした

$dQ = 0$: 断熱過程

$$U_2 - U_1 = +P_1V_1 - P_2V_2$$

$$U_1 + P_1V_1 = U_2 + P_2V_2$$

$$H_1 = H_2$$

等エンタルピー過程

internal energy

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等エンタルピー過程

何の変数で全微分形を書いてよい！

UP THAS VGで書く変数(自然な変数) を使うのが
BEST !

$$dH = TdS + VdP$$

$$H = H(S, P)$$

$$H = H(T, P) \rightarrow \mu_{JT}$$

↑ S が $S(T, P)$ であればOK

理想気体のSは、以下のように書かれる

$$S(T, V) = C_V \ln \frac{T}{T^*} + nR \ln \frac{V}{V^*}$$

* : a reference state

$$PV = nRT, \quad P^*V^* = nRT^*$$

$$S(T, P) = C_V \ln \frac{T}{T^*} + nR \ln \left(\frac{nRT}{P} \frac{P^*}{nRT^*} \right)$$

$$= (C_V + nR) \ln \frac{T}{T^*} + nR \ln \frac{P^*}{P}$$

$$= C_P \ln \frac{T}{T^*} - nR \ln \frac{P}{P^*}$$

↑SはS(T,P)で示された

P一定でTを変化するのとP一定でSを変化は同じ

$H(P, T) :$

$$dH = \left(\frac{\partial H}{\partial P} \right)_T dP + \left(\frac{\partial H}{\partial T} \right)_P dT = 0$$

$$\mu_{JT} \equiv \left(\frac{\partial T}{\partial P} \right)_H = - \left(\frac{\partial H}{\partial P} \right)_T / \underbrace{\left(\frac{\partial H}{\partial T} \right)_P}_{=C_P}$$

$$dH = TdS + VdP$$

$$\left(\frac{\partial H}{\partial P} \right)_T = T \left(\frac{\partial S}{\partial P} \right)_T + V$$

$$dG = VdP - SdT \rightarrow \left(\frac{\partial S}{\partial P} \right)_T = - \left(\frac{\partial V}{\partial T} \right)_P$$

$$\left(\frac{\partial H}{\partial P} \right)_T = -T \left(\frac{\partial V}{\partial T} \right)_P + V = -T \frac{nR}{P} + V = 0$$

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別解

$$dH = TdS + VdP$$

$$S = S(T, P)$$

$$dS = \left(\frac{\partial S}{\partial T} \right)_P dT + \left(\frac{\partial S}{\partial P} \right)_T dP$$

$$dH = T \left(\frac{\partial S}{\partial T} \right)_P dT + \left[T \left(\frac{\partial S}{\partial P} \right)_T + V \right] dP$$

$$TdS = dQ, \quad T \left(\frac{\partial S}{\partial T} \right)_P = C_P dT$$

$$dG = -SdT + VdP \rightarrow \left(\frac{\partial S}{\partial P} \right)_T = - \left(\frac{\partial V}{\partial T} \right)_P$$

$$dH = C_P dT + \left[-T \left(\frac{\partial V}{\partial T} \right)_P + V \right] dP$$

$$\mu_{\text{JT}} = \left(\frac{\partial T}{\partial P} \right)_H = \left[-T \left(\frac{\partial V}{\partial T} \right)_P + V \right] / C_P$$

$$V = \frac{nRT}{P}, \quad -T \frac{nR}{P} + V = -V + V = 0$$

理想気体では

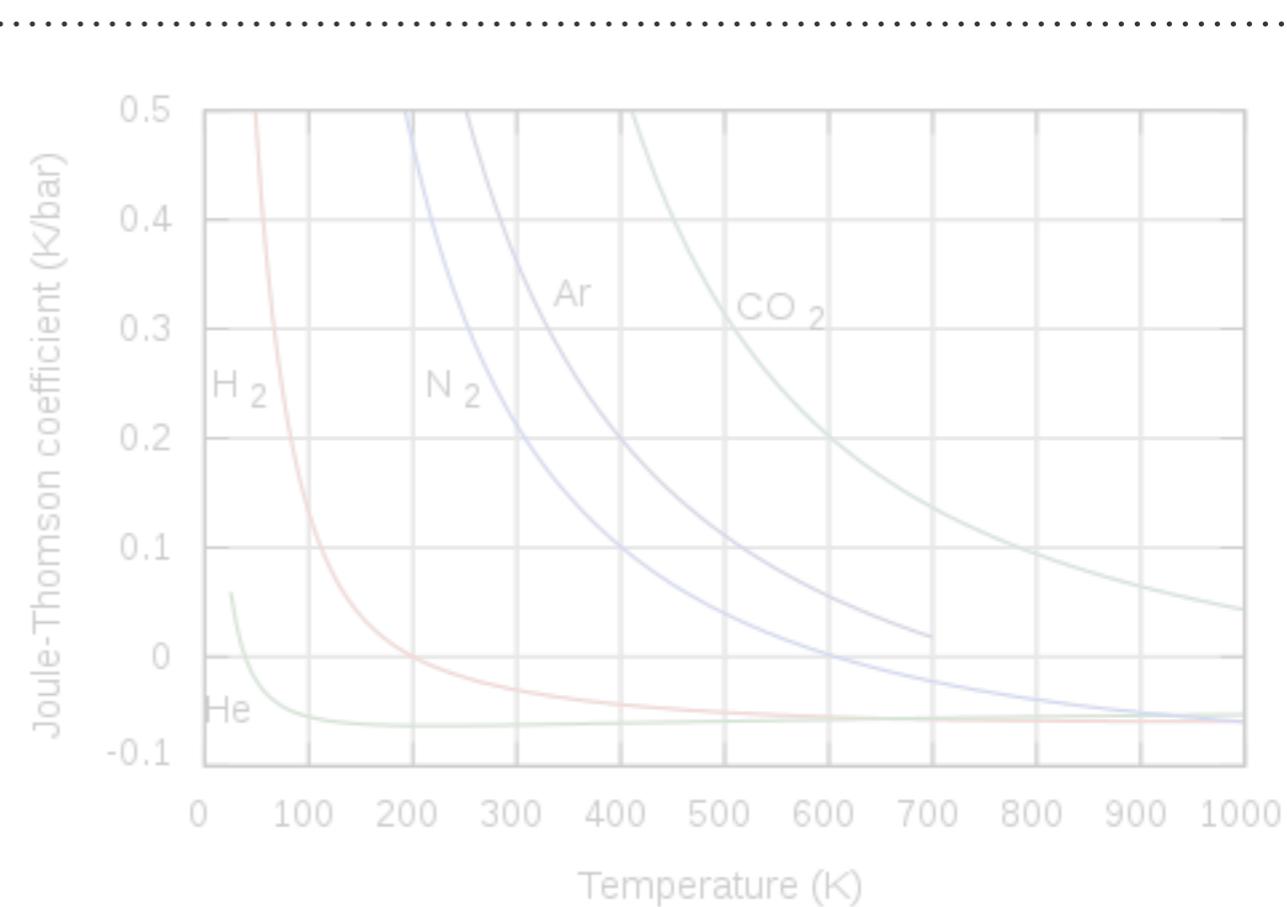
JT過程で

温度は変化しないが

実在気体では下がる

ガスの液化に使われている

https://en.wikipedia.org/wiki/Joule–Thomson_effect



Joule-Thomson coefficients for various gases at atmospheric pressure.

$$P_1 > P_2$$

If the gas temperature is

below the inversion temperature

above the inversion temperature

then μ_{JT} is

positive

negative

since ∂P is

always negative

always negative

thus ∂T must be

negative

positive

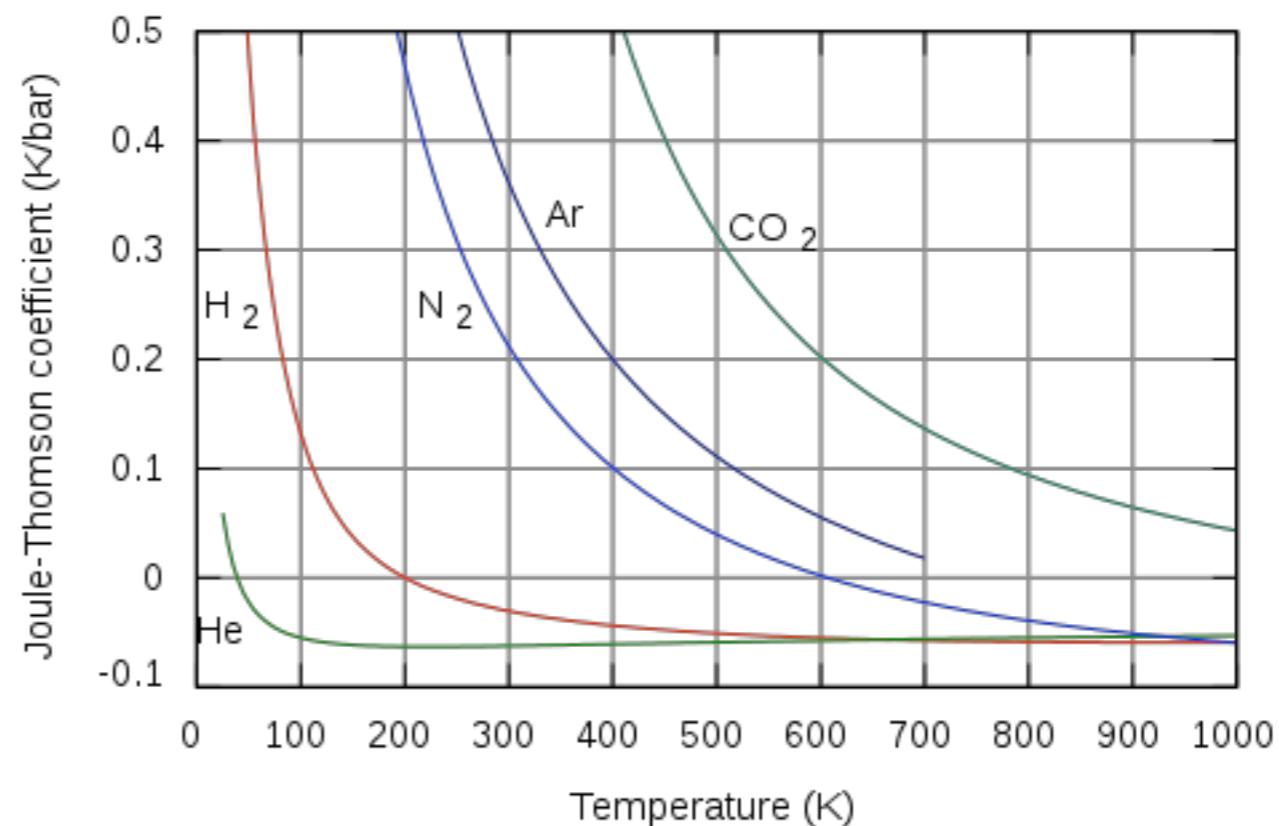
so the gas

cools

warms

For an ideal gas, μ_{JT} is always equal to zero: ideal gases neither warm nor cool upon being expanded at constant enthalpy.

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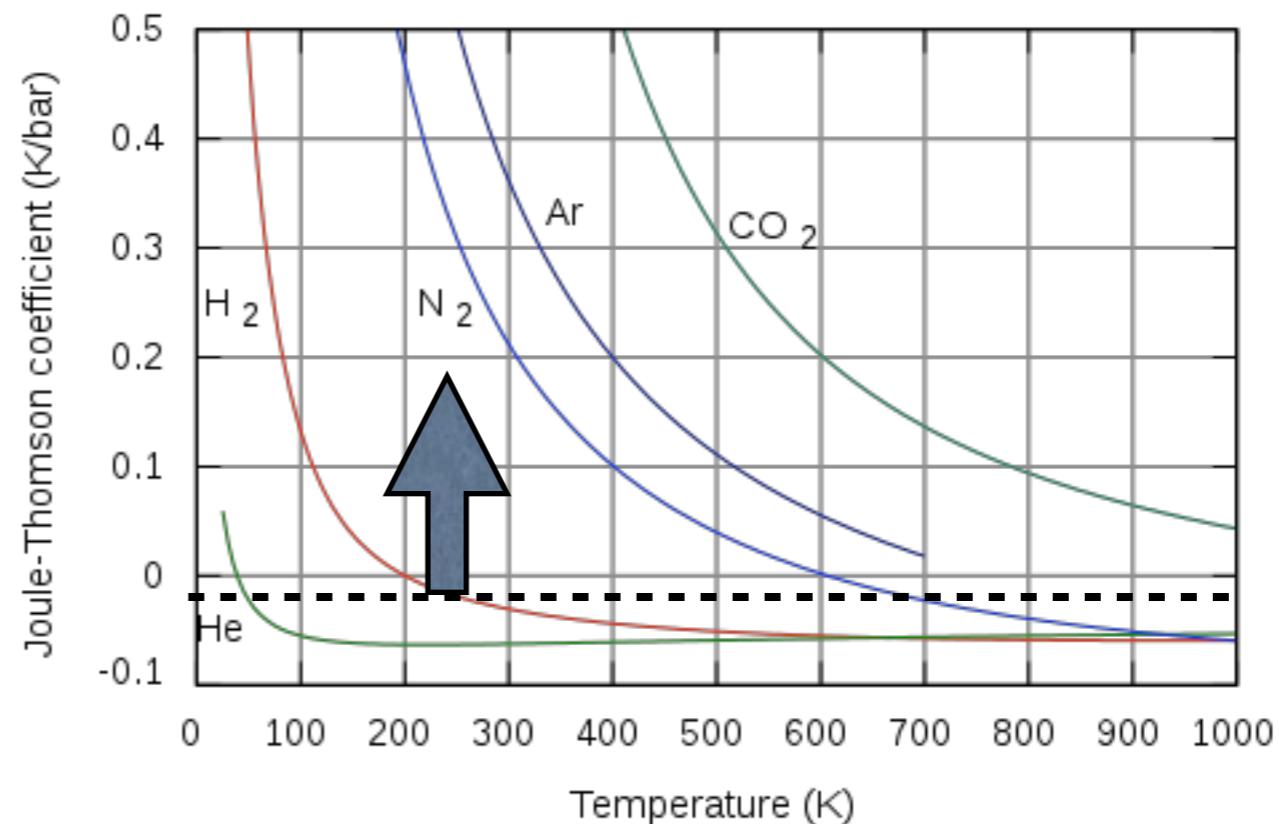
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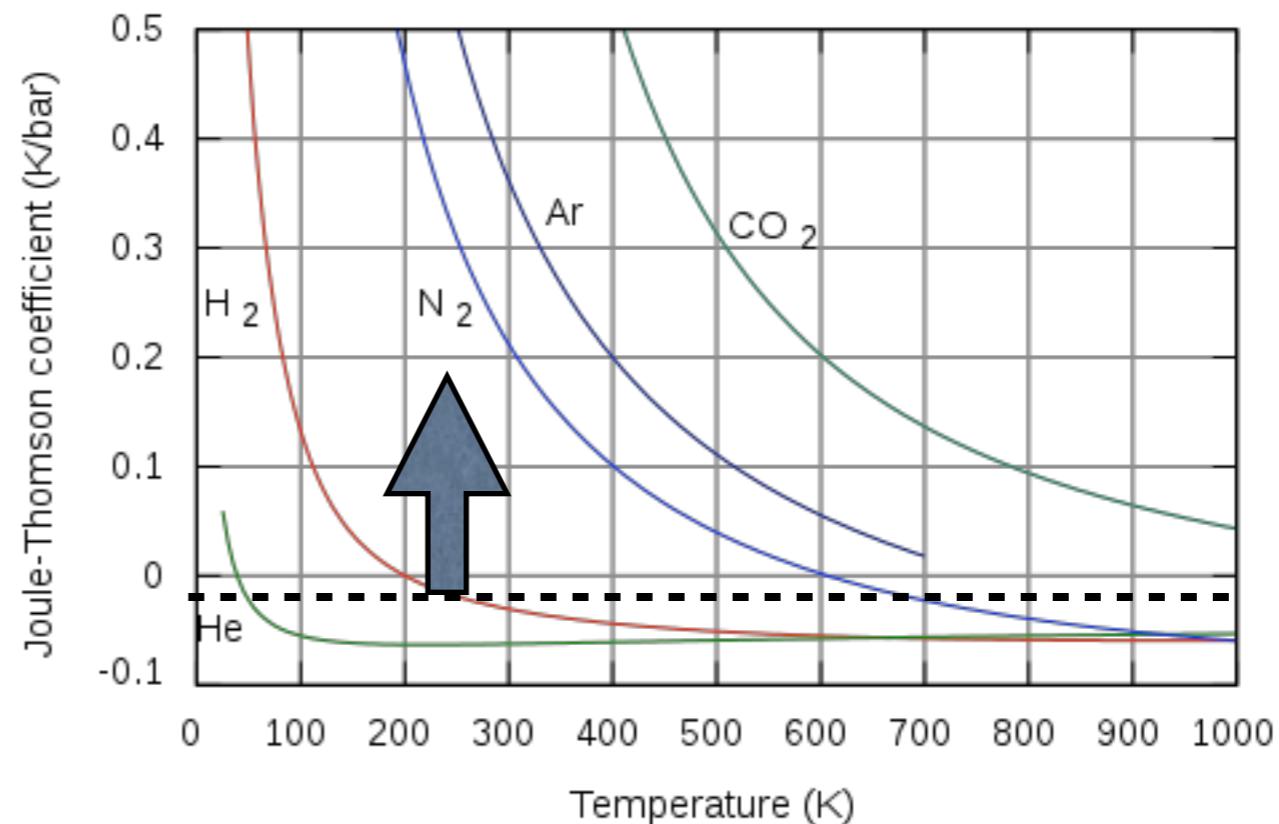
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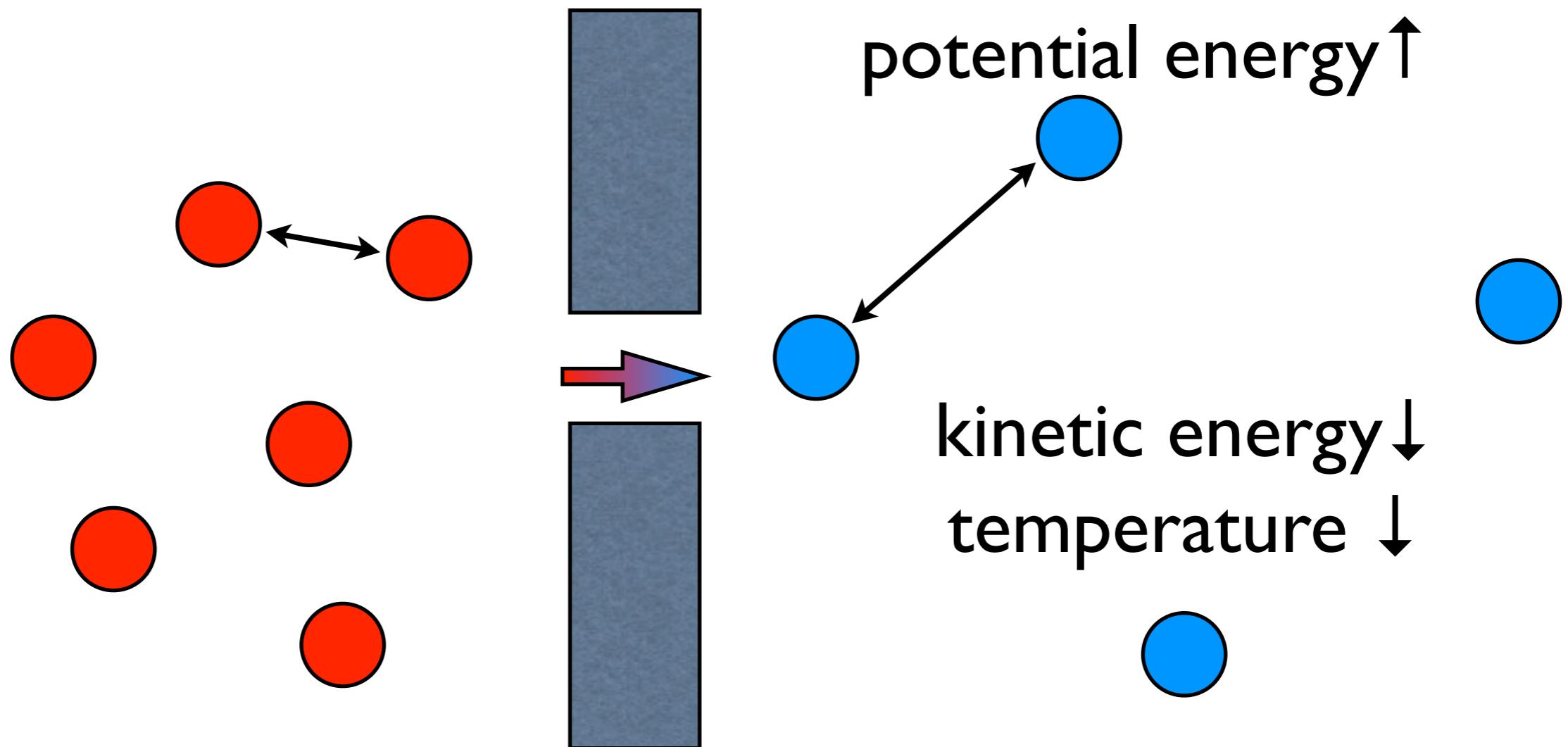
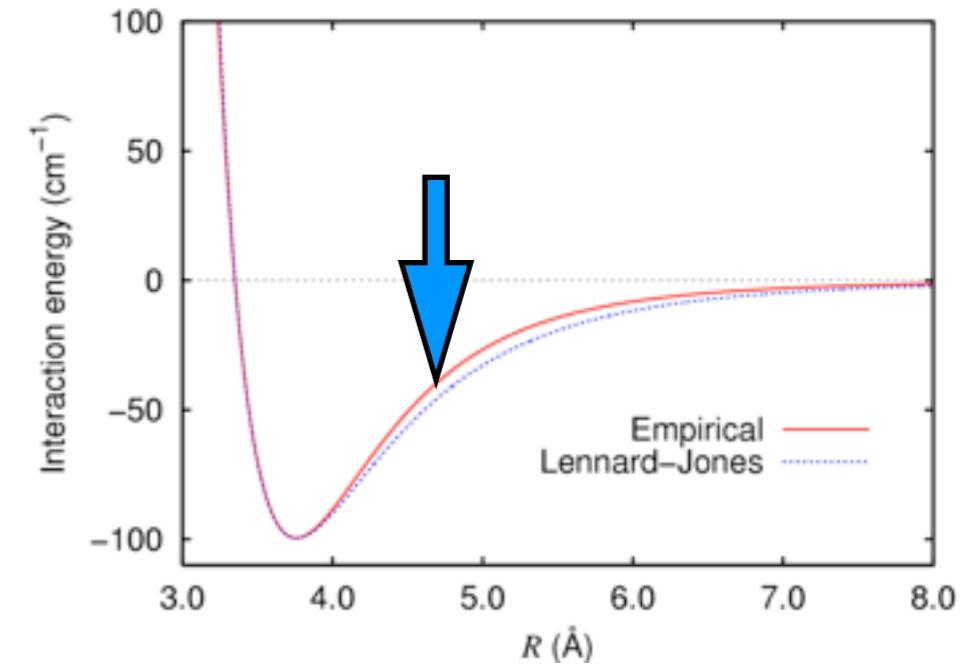
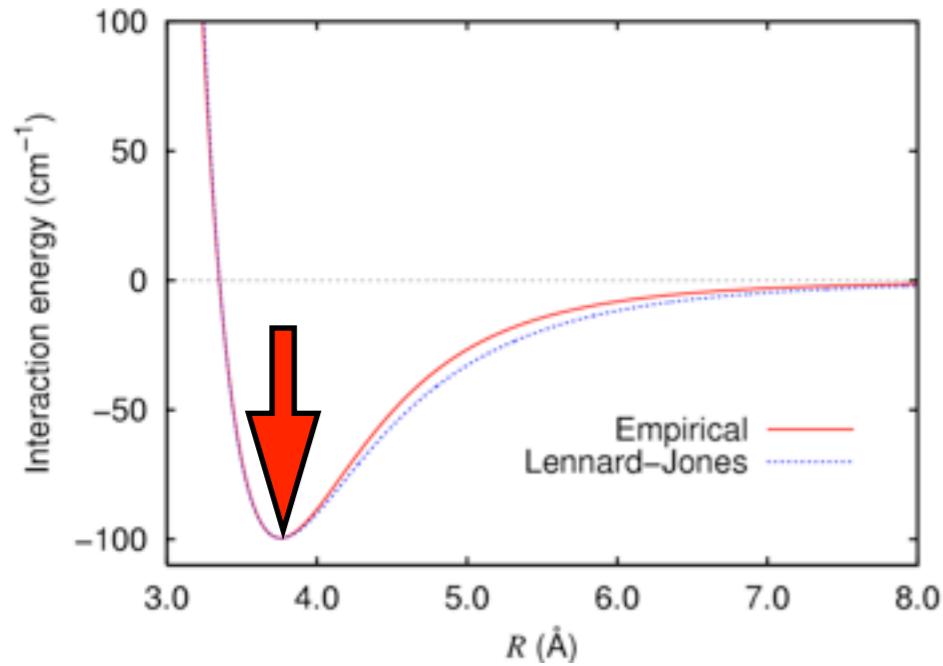
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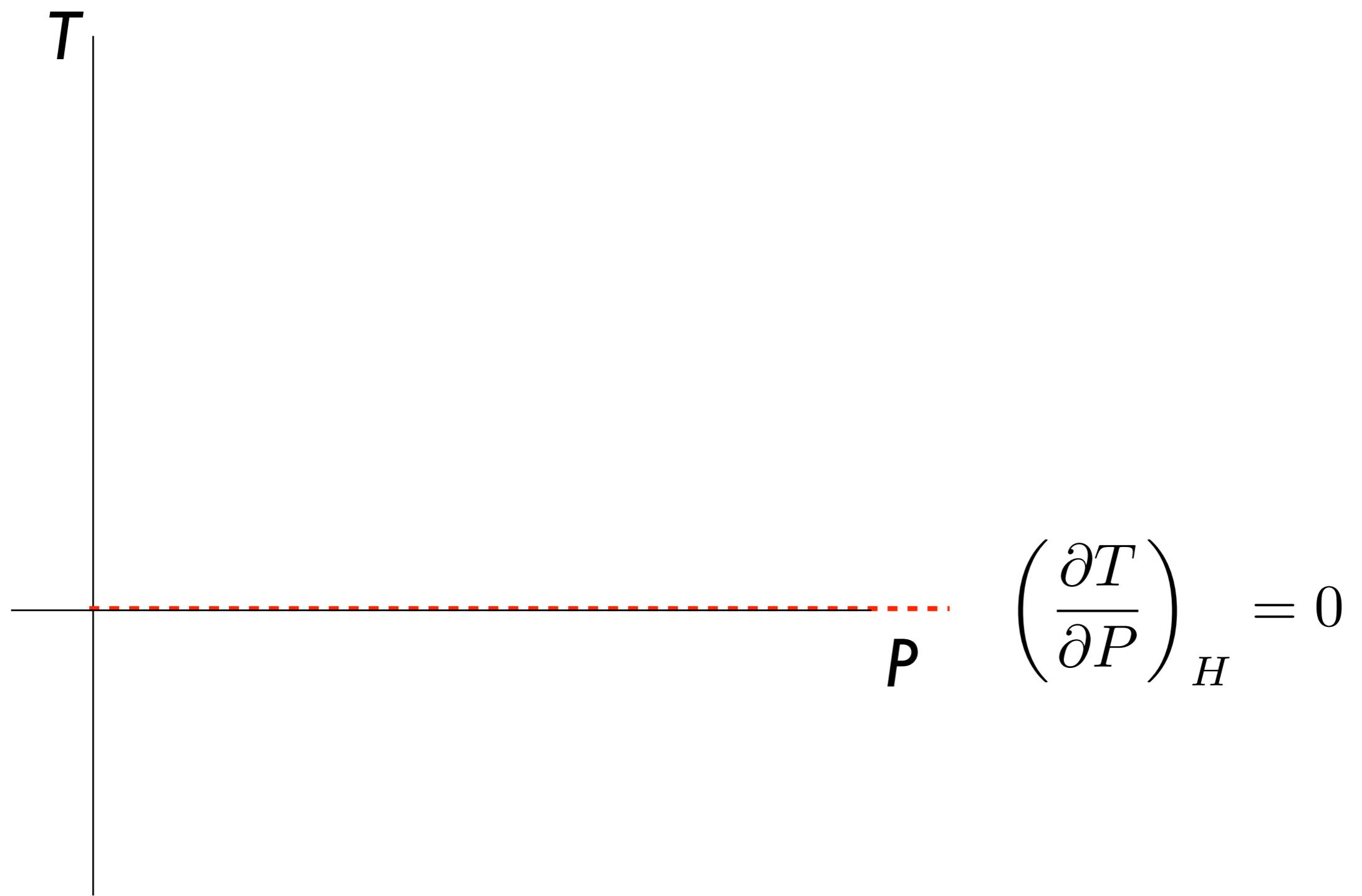
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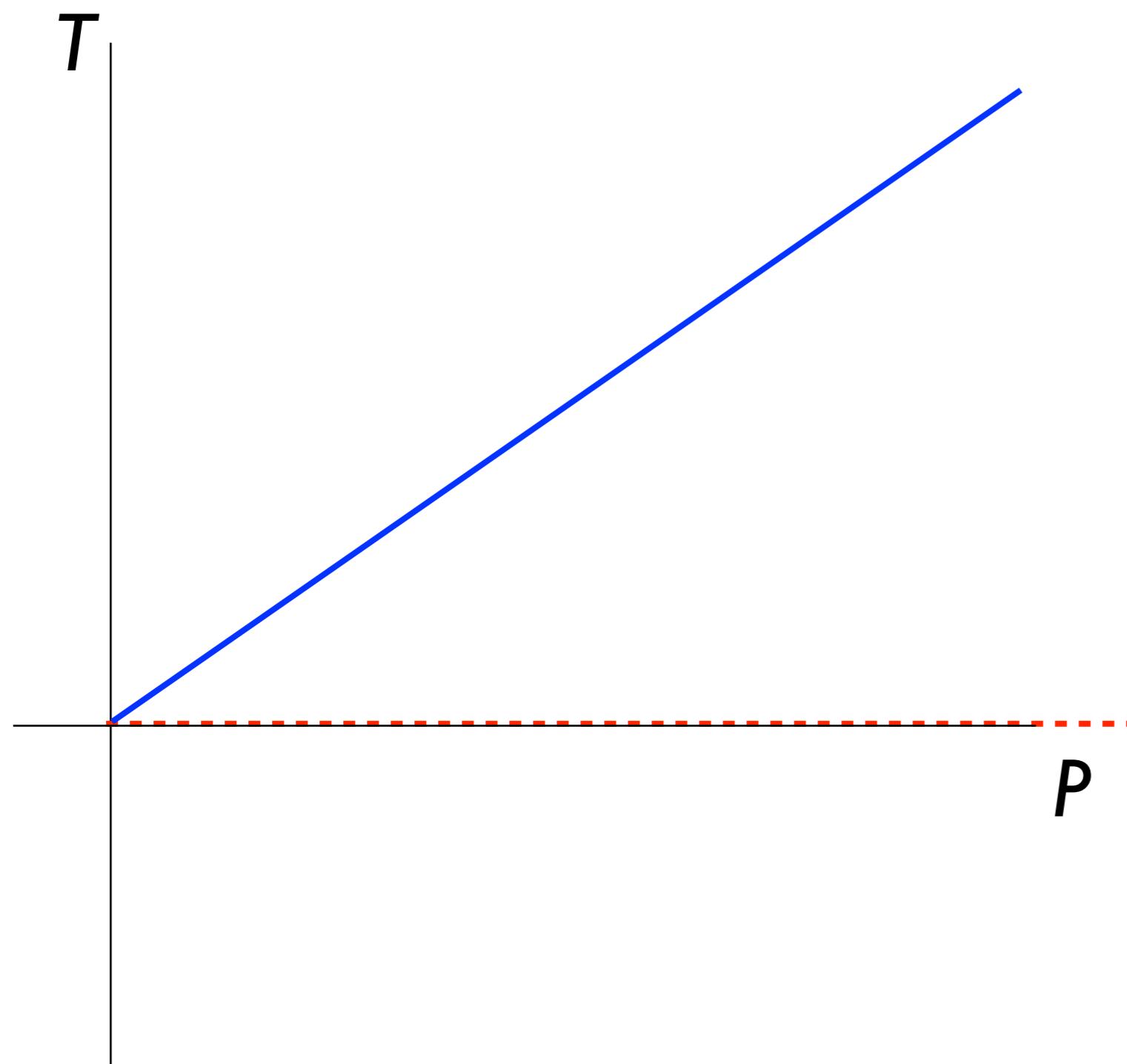


P

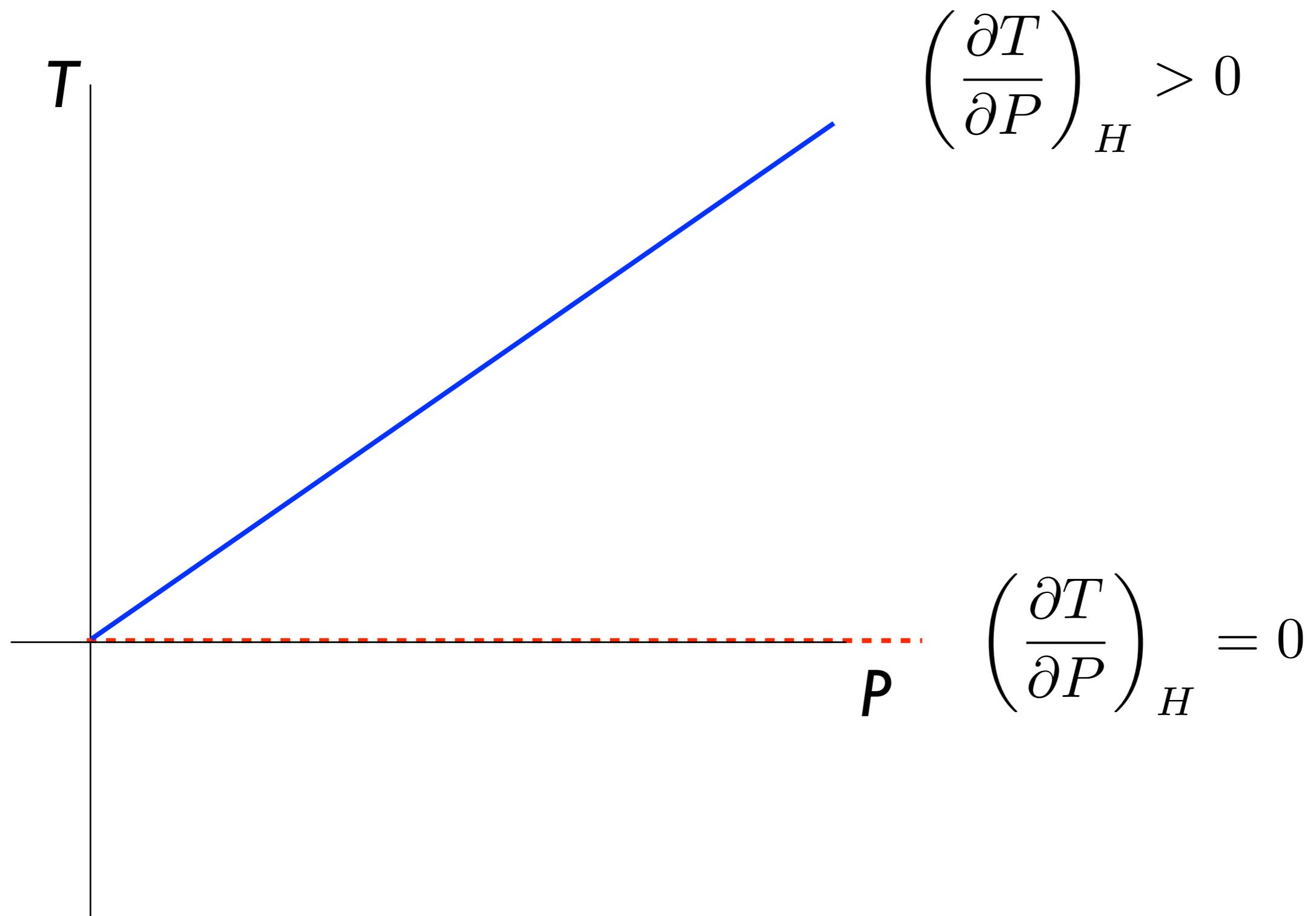
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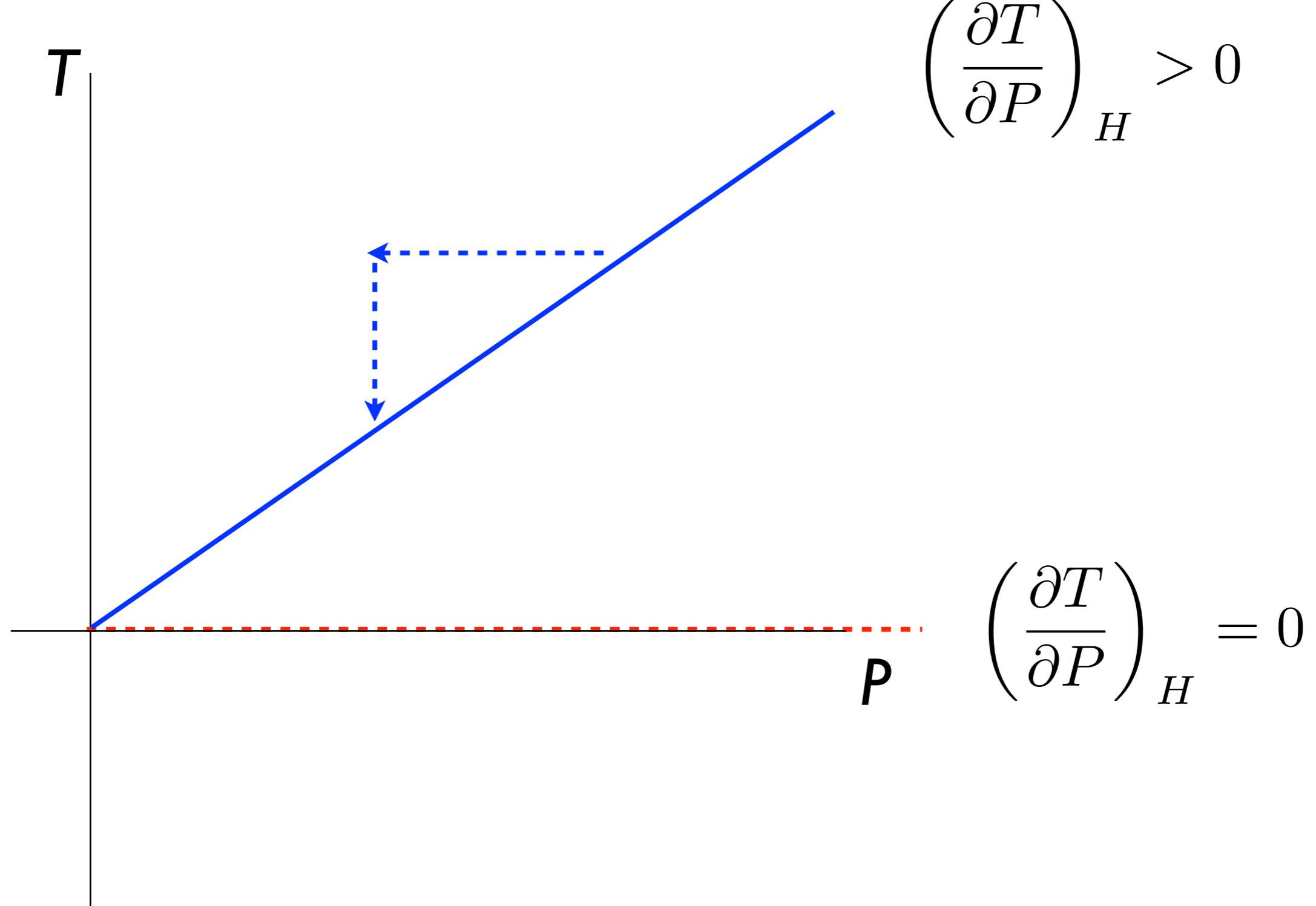
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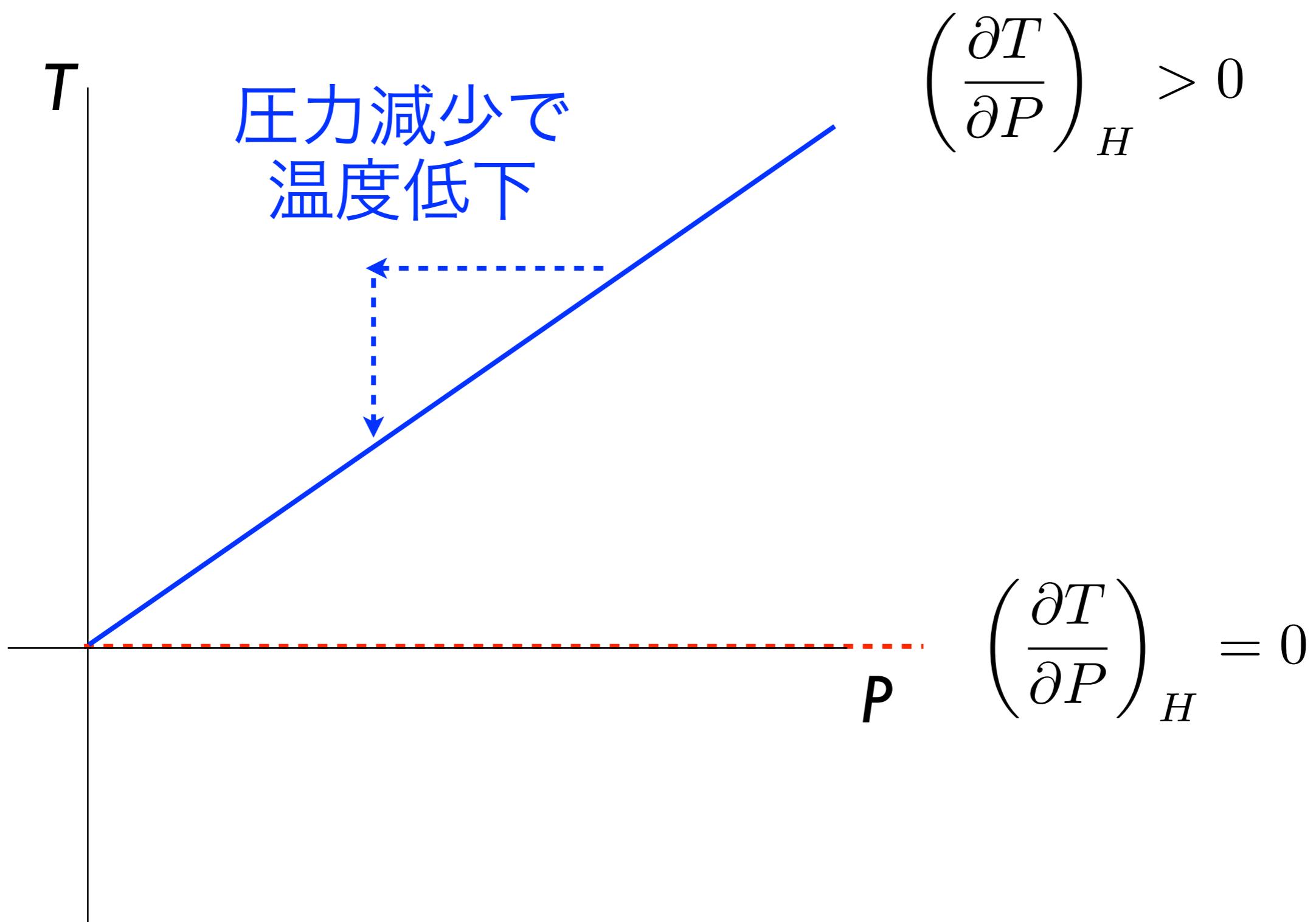


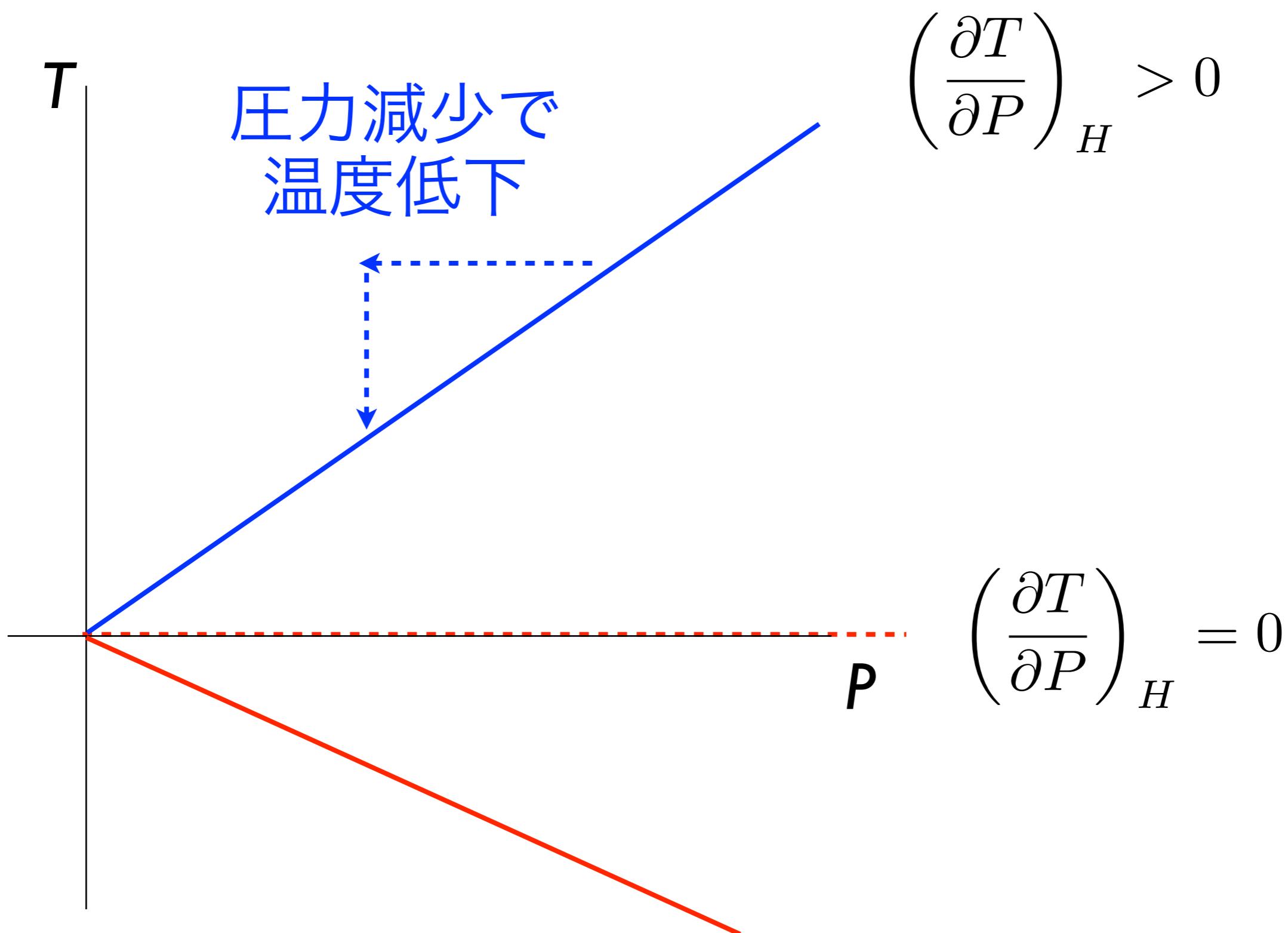


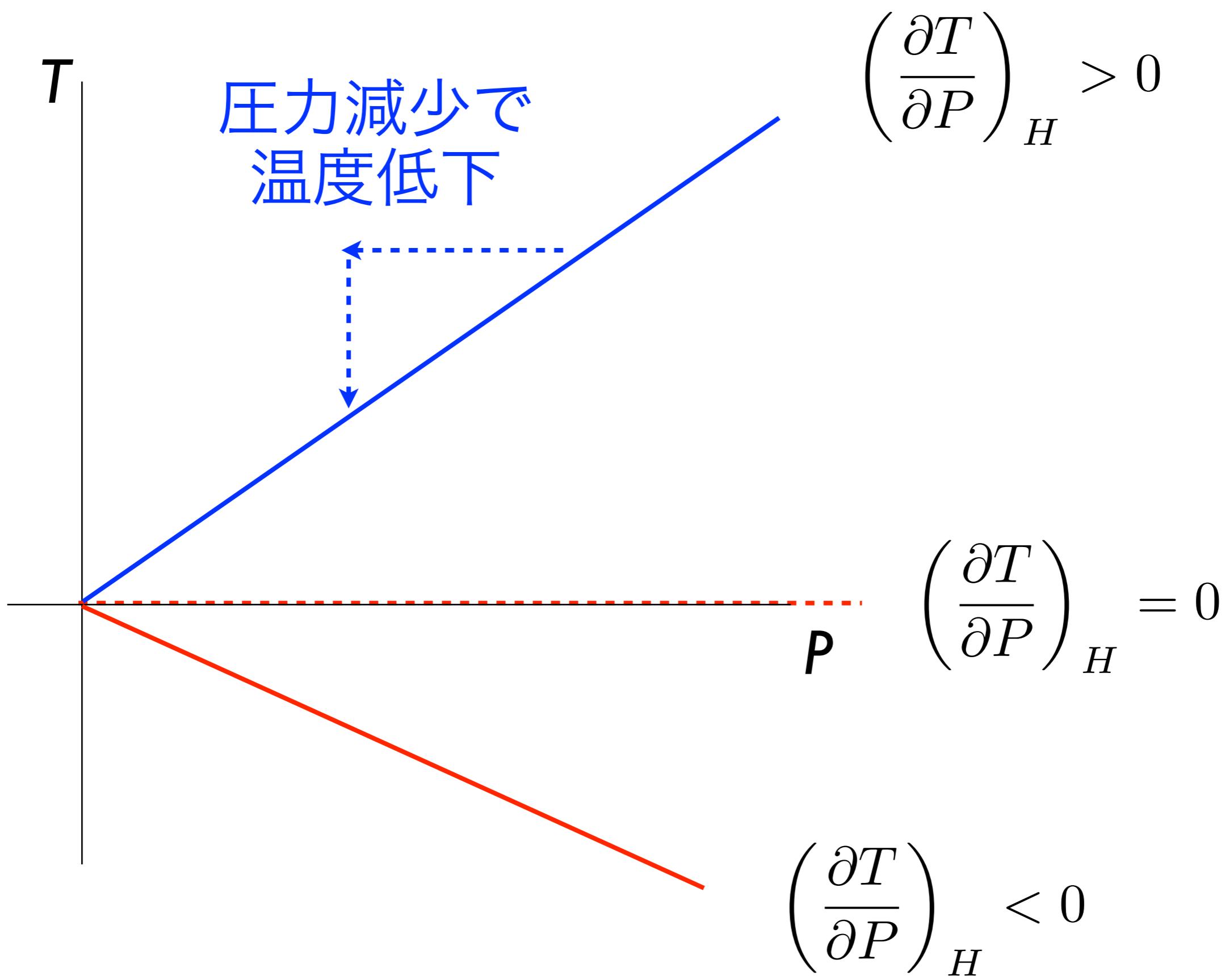
$$\left(\frac{\partial T}{\partial P} \right)_H = 0$$

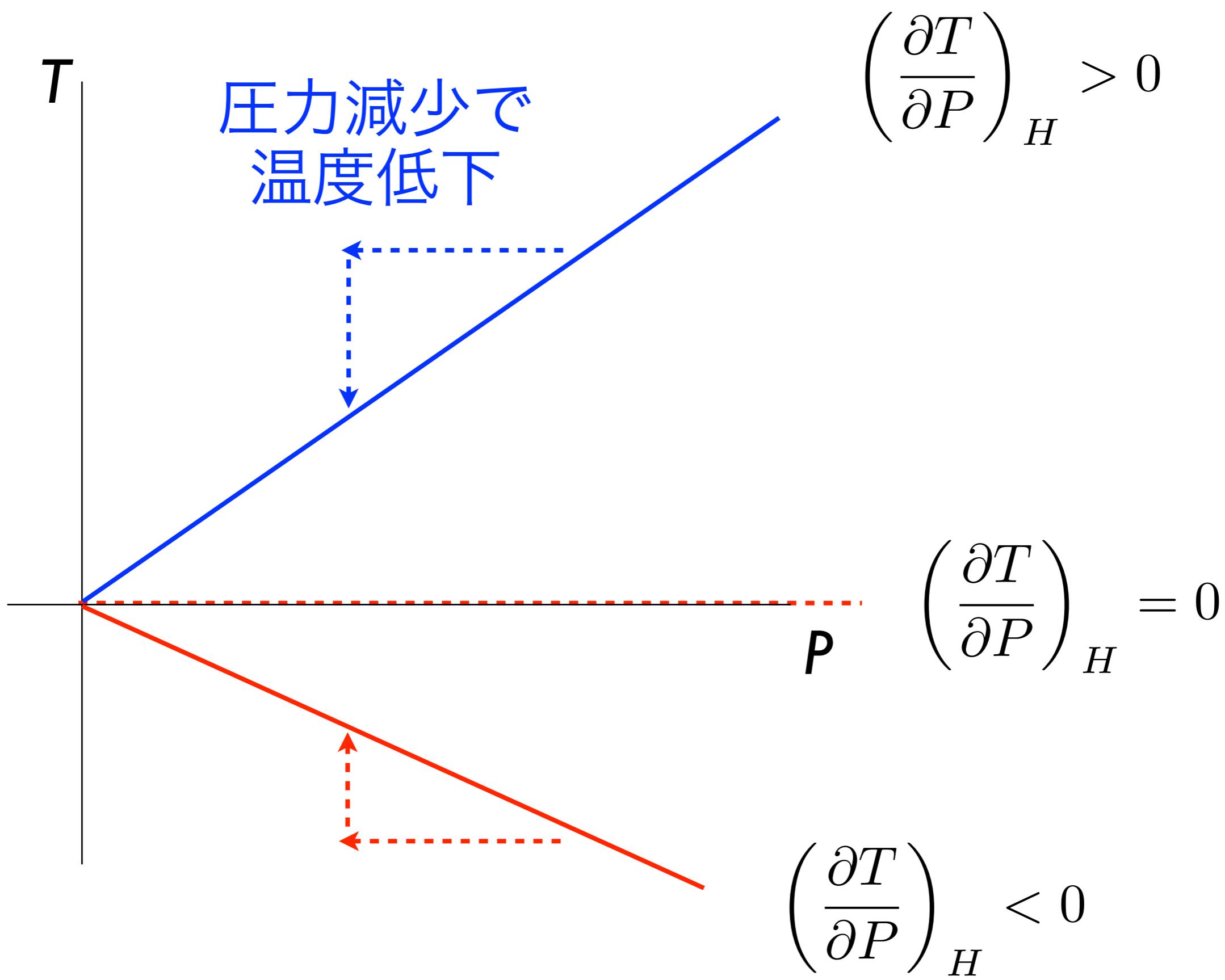


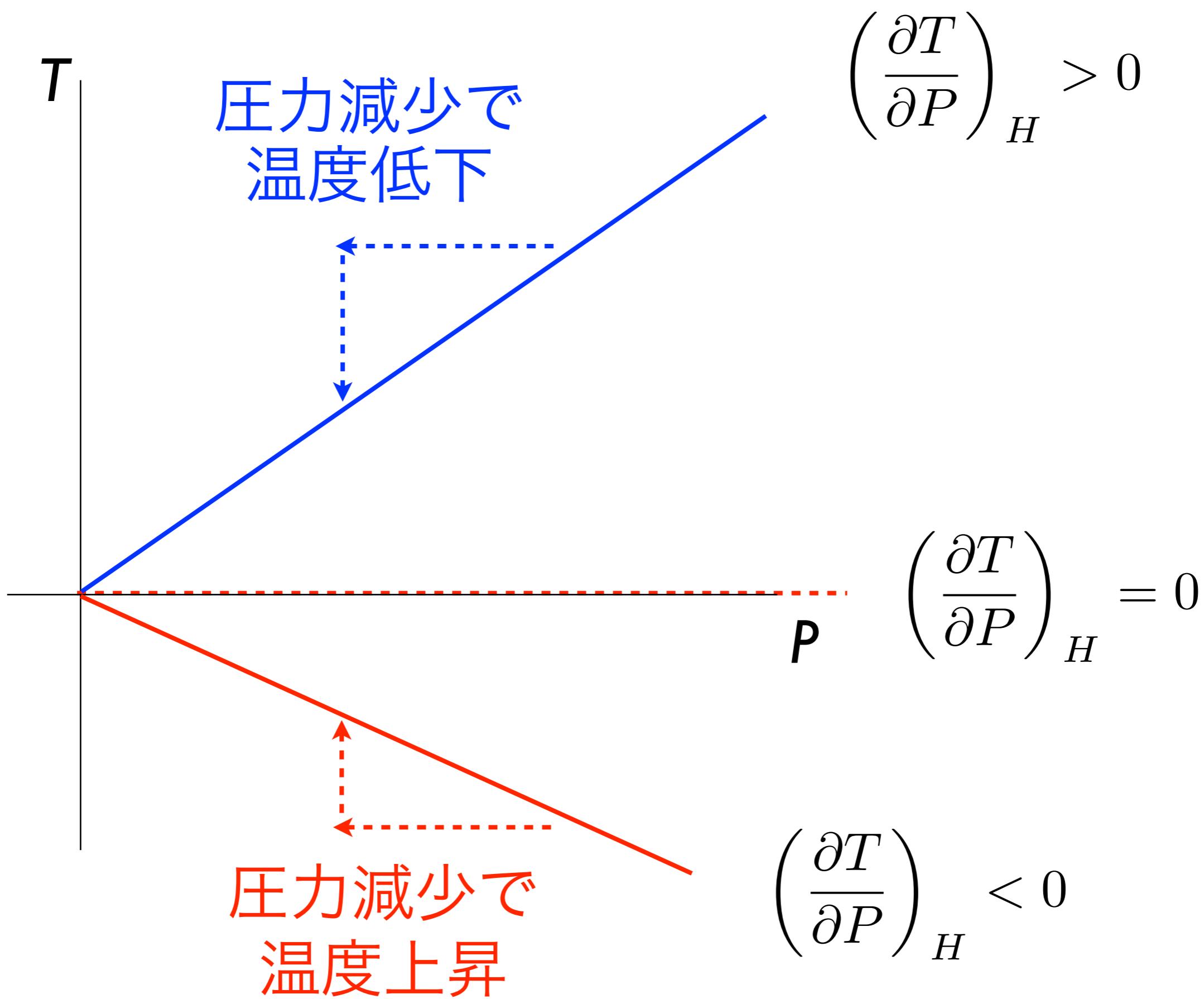












LNG : Liquid Natural gas ($\text{CH}_4, \text{C}_2\text{H}_6, \text{C}_3\text{H}_8, \text{C}_4\text{H}_{10}$)

エタンのJT係数 > 0

Experimental results for heat capacity and Joule-Thomson coefficient of ethane at zero pressure

Konrad Bier, Joachim Kunze, Gerd Maurer, Holger Sand J. Chem. Eng. Data, 1976, 21 (1), pp 5–7 DOI: 10.1021/je60068a033

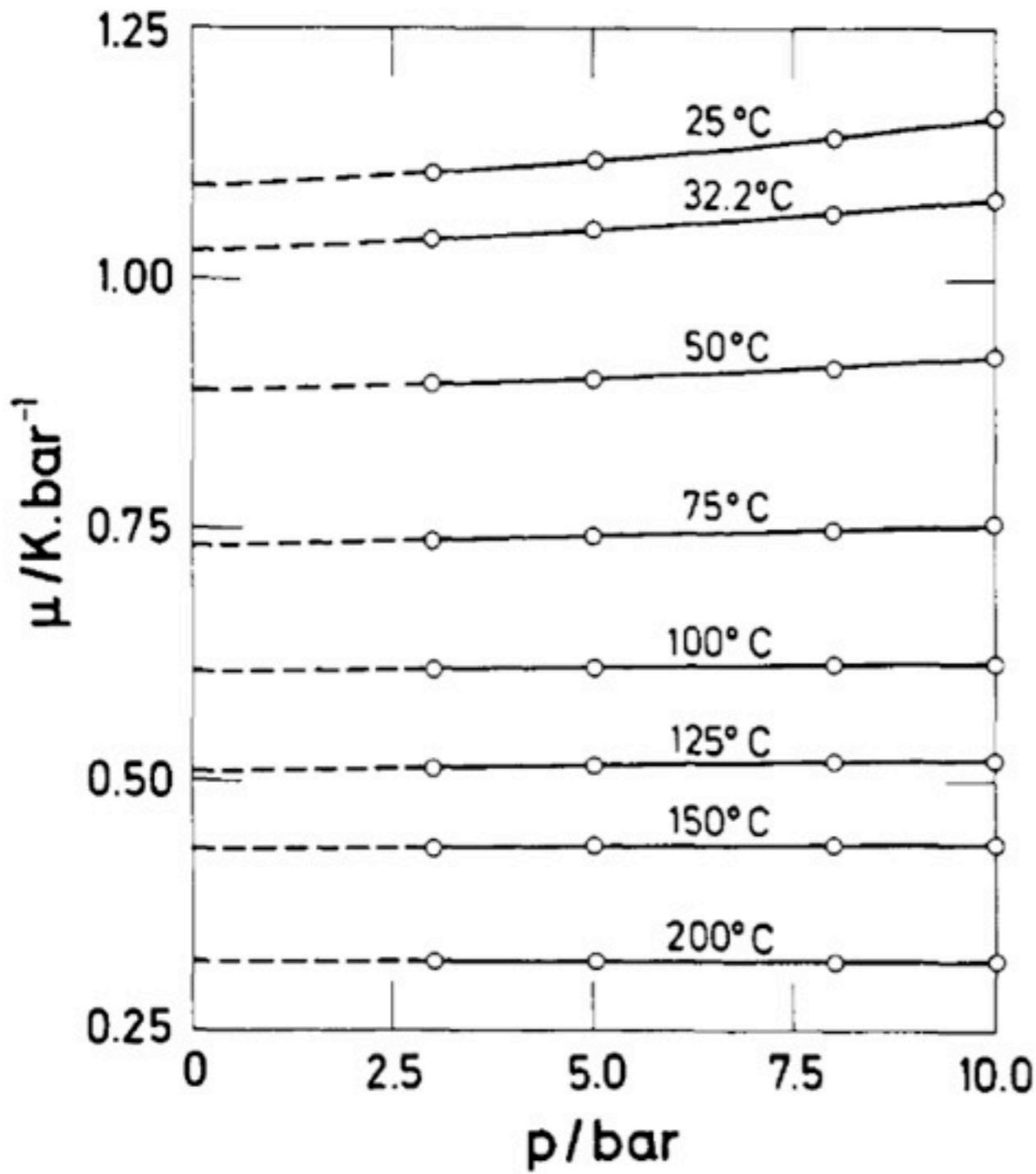


Figure 2. Experimental results for differential Joule-Thomson coefficient of ethane

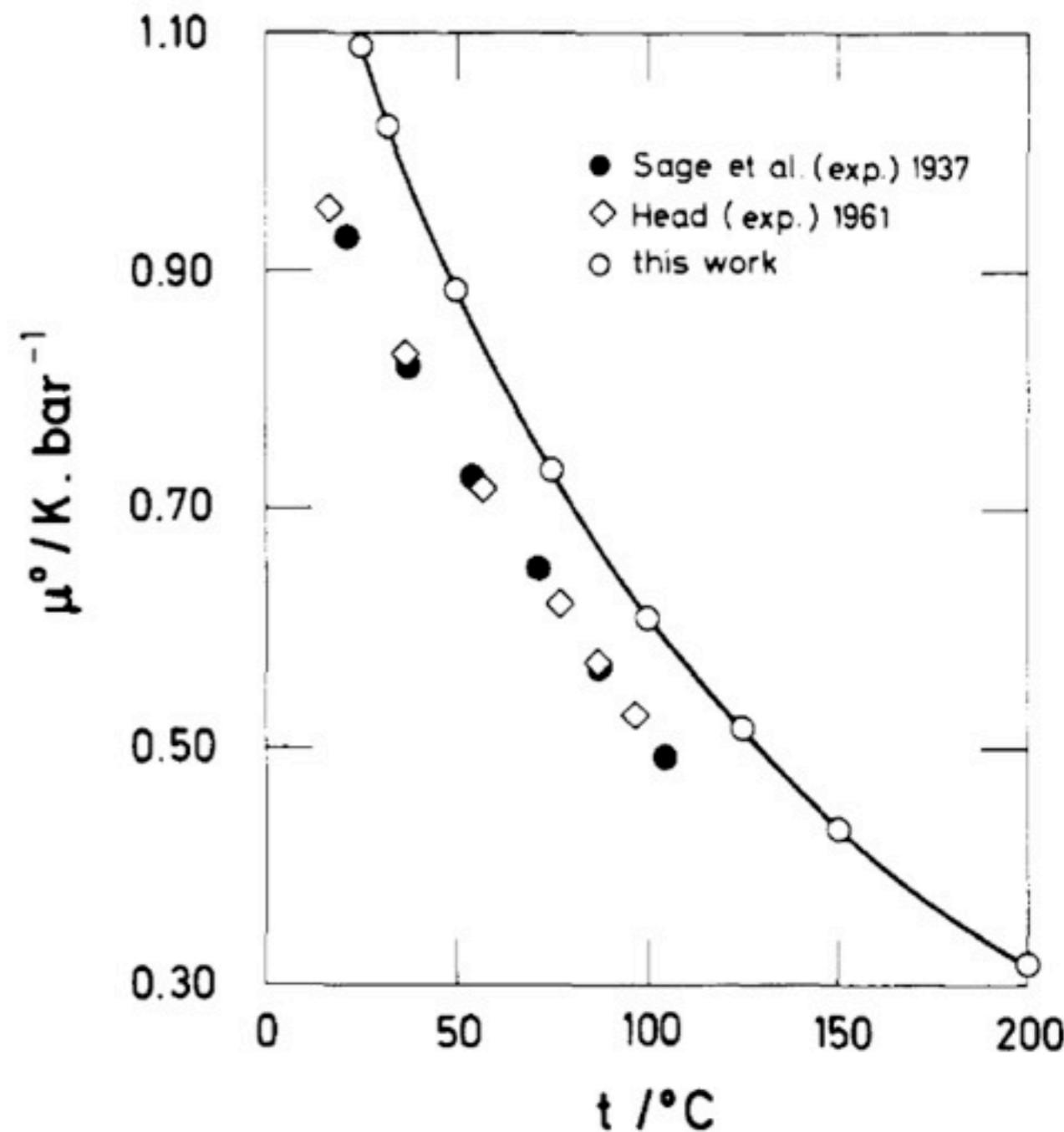


Figure 4. Differential Joule-Thomson coefficient at zero pressure of ethane

天然ガス液化の原理は、気体が膨張して密度が減少するときに、希薄な密度を維持するために内部エネルギーの一部が使用されて温度が低下するという、**ジュール・トムソン効果**を利用するものである

http://oilgas-info.jogmec.go.jp/pdf/0/598/200503_001a.pdf

